73t/hr Natural Gas / Syngas Fuelled Boiler Plant



Year of Manufacture: 2014

Condition: Unused

Operating Hours: 0 (Never Operated)

Status: Installed

Fuel: NG/Syngas

Basic Information:

The Boiler is equipped with selective catalytic reduction (SCR), where aqueous ammonia is injected for NOx reduction. Flue gases exiting the stack are continually monitored by way of the continuous emissions monitoring system (CEMS). The CEMS monitors compliance with environmental regulations.

Manufacturer: RENTECH Year of Manufacture: 2014 Fuel: Syngas/Natural Gas Steam Capacity: 73t/hr

Steam Temperature: 400 Deg C

Steam Pressure: 45 Bar



| Furnace Input Data | | | Calculated Results | | |
|--------------------------|--------|----------|--------------------------|--------|----------|
| Fuel Type | Gas | | Heat Losses: | | |
| Furnace Duty | 193.20 | MM Btu/h | Dry Gas Loss | 4.47 | 8 |
| Radiation Heat Loss | 0.50 | 8 | Air Moisture | 0.12 | 8 |
| Unaccountable Heat Loss | 1.50 | 8 | Fuel Moisture | 10.32 | 8 |
| Ambient Air Temperature | | | Radiation (input) | 0.50 | |
| Relative Humidity | 60.0 | 8 | Unaccountable (input) | 1.50 | 8 |
| Excess Air | 15.0 | 8 | | 91.81 | |
| Exit Gas Temperature | 318 | F | Efficiency HHV | 83.09 | 8 |
| Gas Recirculation | 0.0 | 8 | Flue Gas Analysis, by Vo | olume: | |
| Steam Temperature | 752 | | Carbon Dioxide | 8.68 | 8 |
| Steam Pressure | 696.0 | psig | Water Vapor | 17.70 | 8 |
| Steam Flow Rate | 160937 | pph | Nitrogen | 71.15 | 8 |
| Feed Water Temperature | 219 | F | Oxygen | 2.46 | 8 |
| Furnace Length | 37.30 | feet | Sulfur Dioxide | 0.00 | 8 |
| Furnace Height | 11.00 | feet | Furnace Volume | 3077.2 | cu.ft. |
| Furnace Width | 7.50 | feet | Furnace Surface | 1523.9 | sq.ft. |
| Tube Diameter | 2.0 | inch | Furnace Duty | 63.39 | MM Btu/h |
| | | | Furnace Temperature | 2357 | F |
| Fuel Analysis, by Volume | 2: | | Mixture Temperature | 80 | F |
| Methane | 85.41 | 8 | Higher Heating Value | 22050 | Btu/lb |
| Ethane | 7.49 | 8 | Lower Heating Value | 19957 | Btu/lb |
| Propane | 2.67 | 8 | Higher Heating Value | 1114 | Btu/scf |
| Butane | 1.34 | 8 | Lower Heating Value | 1008 | Btu/scf |
| Pentane | 0.00 | 8 | Fuel Flow Rate | 10545 | pph |
| Ethylene | 0.00 | 8 | Air Flow Rate | 194708 | pph |
| Propylene | 0.00 | 8 | Flue Gas Flow Rate | 205252 | pph |
| Butylene | 0.00 | 8 | FGR Flow Rate | 0 | pph |
| Benzene | 0.00 | 8 | Total Gas Flow Rate | 205252 | pph |
| Tolyne | 0.00 | 8 | lb/lb Air | 18.47 | |
| Acetylene | 0.00 | 8 | lb/lb Gas | 19.47 | |
| Ammonia | 0.00 | 8 | Heat Release (HHV) | 74046 | Btu/cfh |
| Hydrogen Sulfide | 0.00 | 8 | Heat Release (HHV) | 149522 | Btu/sfh |
| Water Vapor | 0.00 | 8 | Heat Release (LHV) | 67018 | Btu/cfh |
| Nitrogen | 1.05 | 8 | Heat Release (LHV) | 135331 | Btu/sfh |
| Carbon Dioxide | 2.04 | 8 | Fuel HHV | 232.51 | MM Btu/h |
| Carbon Monoxide | 0.00 | 8 | Heat Flux | 41594 | Btu/sfh |
| Hydrogen | 0.00 | 8 | ASME Surface | 1920.1 | sq.ft. |
| Sulfur Dioxide | 0.00 | 8 | Recirculation duct area | 0.000 | sq.ft. |
| | | | Recirculation duct diam | 0.00 | inches |
| | | | | | |

| Gas Data, Case 1 | | | | | | |
|---|---|--|--|--|--|--|
| Boiler Input Data Calculated Results | | | | | | |
| Gas Flow Rate In: 205252 pph | | | | | | |
| <u>-</u> | Gas Pressure Drop: 10.312 in H20 | | | | | |
| | Gas In Molecular Mass: 27.73 | | | | | |
| Gas Cleanness: Clean | n | | | | | |
| Gas Inlet Composition by Volume: CO2: 8.680 % H2S: 0.000 % | Extra Gas-Side Pressure Drops: SCR/CO Pressure Drop: 0.000 in H20 | | | | | |
| H2O: 17.700 % H2: 0.000 % | • • • • • • • • • • • • • • • • • • • | | | | | |
| N2: 71.150 % CO: 0.000 % | Burner Pressure Drop: 0.000 in H2O Stack Pressure Drop: 0.000 in H2O | | | | | |
| 02: 2.460 % CH4: 0.000 % | Misc. Pressure Drop: 0.000 in H20 | | | | | |
| 02: 2.460 € CR4: 0.000 € | Total Gas-Side Extra | | | | | |
| SO2: 0.000 % SO3: 0.000 % HCl: 0.000 % Ar: 0.000 % | | | | | | |
| Number of Groups: 1 | Pressure Drop: 0.000 in H20 | | | | | |
| Burner Section: 0 | | | | | | |
| Burner Section: U | | | | | | |
| Group 1 | | | | | | |
| | Steam Exit Flow Rate: 160929 pph | | | | | |
| Economiser Flow Rate: 0 pph | | | | | | |
| External Evap Flow Rate: 0 pph | | | | | | |
| Blow Down Factor: 3.0 % | Blow Down Flow Rate: 4929 pph | | | | | |
| Spray Temperature: 219 F | Spray Flow Rate: 1544 pph | | | | | |
| Design Steam Temperature: 752 F | Steam Exit Temperature: 752 F | | | | | |
| FW Inlet Temperature: 219 F | Saturation Temperature: 514 F | | | | | |
| | Water Pressure Drop: 65.18 psi | | | | | |
| Steam Pressure: 710.7 psia | Drum Operating Pressure: 769.3 psia | | | | | |
| External Radiation Duty: 63.390 MMB/h | | | | | | |
| Heat Loss: 0.0 % | | | | | | |
| Extra Water-Side Pressure Drops: | Total Group Duty: 192.239 MMB/h | | | | | |
| Steam Drum to De-SH: 5.00 psi | | | | | | |
| De-SH Piping: 5.00 psi | Pressure Drop: 22.00 psi | | | | | |
| De-SH: 5.00 psi | | | | | | |
| Non-Return Valve: 7.00 psi | Number of Furnace Sections: 0 | | | | | |
| Number of Sections: 5 | Number of Screens: 1 | | | | | |
| Spray Between Sections 2 & 0 | Number of Superheaters: 1 | | | | | |
| Water Enters from Section: 5 | Number of Evaporators: 2 | | | | | |
| Water Exits from Section: 2 | Number of Economizers: 1 | | | | | |
| Screen Section | l. Group 1 | | | | | |
| Tube Outside Diameter: 2.000 in | Tube Inside Diameter: 1.706 in | | | | | |
| Tube Min Wall Thickness: 0.135 in | Gas Inlet Temperature: 2357 F | | | | | |
| Tube Length: 10.50 ft | Gas Outlet Temperature: 2272 F | | | | | |
| Finned Tube Length: 10.50 ft | Water Inlet Temperature: 371 F | | | | | |
| Tube ASME Material Group: B | Water Outlet Temperature: 514 F | | | | | |
| Number of Tubes Wide: 13 | Max Tube Temp (qas in): 659 F | | | | | |
| Number of Tubes Deep: 2 | Mean Wall Temperature: 643 F | | | | | |
| Fin Margin Temp Diff: 0 F | Max Fin Tip Temperature: 659 F | | | | | |
| Transverse Pitch: 4.750 in | Gas PD Surface Area: 143 sft | | | | | |
| Longitudinal Pitch: 4.000 in | Gas Pressure Drop: 0.194 in H20 | | | | | |
| Tube Arrangement: Inline | Water Pressure Drop: 0.000 psi | | | | | |
| Flow Direction: | Maximum Gas Velocity: 135.1 ft/s | | | | | |
| Number of Streams: 0 | Gas Specific Heat: 0.338 B/lb-F | | | | | |
| Outside Fouling Factor: 0.0010 | Overall HT Coef (U): 22.91 B/h-sf-F | | | | | |
| Inside Fouling Factor: 0.0010 | Mean Temperature Dif: 1800 F | | | | | |
| Number Fins per inch: 0.00 | Gas HTC (hc): 20.00 B/h-sf-F | | | | | |
| Fin Height: 0.000 in | Radiant HTC (hn): 20.00 B/h Sf F | | | | | |
| Fin Thickness: 0.000 in | Water HTC (hi): 2000.00 B/h-sf-F | | | | | |
| Fin Serrated Factor: 0.000 | Convection Duty: 5.895 MMB/h | | | | | |
| Fin ASME Material Group: | Maximum Heat Flux: 49510 Btu/sf | | | | | |
| Water In From Section: 5 | Total Section Duty: 69.285 MMB/h | | | | | |
| Water Out To Section: 2 | Trace Section Pasy. 05.200 Help/H | | | | | |
| NECT OUT IS SECTION. | | | | | | |

Superheater Section 2, Group 1

| Tube Outside Diameter: | 2.000 | in | Tube Inside Diameter: | 1.673 | in |
|---------------------------|---------|----|---------------------------|--------|----------|
| Tube Min Wall Thickness: | 0.150 | in | Gas Inlet Temperature: | 2272 | F |
| Tube Length: | 4.75 | ft | Gas Outlet Temperature: | 1837 | F |
| Tube ASME Material Group: | C | | Water Inlet Temperature: | 514 | F |
| Number of Tubes Wide: | 22 | | Water Outlet Temperature: | 772 | F |
| Number of Tubes Deep: | 16 | | Max Tube Temp (gas out): | 957 | F |
| Fin Marginal Temp Diff: | 0 | F | Mean Wall Temperature: | 944 | F |
| Transverse Pitch: | 4.500 | in | Max Fin Tip Temperature: | 957 | F |
| Longitudinal Pitch: | 4.000 | in | Gas PD Surface Area: | 875 | sft |
| Tube Arrangement: | Inline | | Gas Pressure Drop: | 3.036 | in H2O |
| Flow Direction: Pa | arallel | | | | |
| Number of Streams: | 22 | | Maximum Gas Velocity: | 188.3 | ft/s |
| Outside Fouling Factor: | 0.0010 | | Gas Specific Heat: | 0.332 | B/lb-F |
| Inside Fouling Factor: | 0.0010 | | Overall HT Coef (U): | 24.46 | B/h-sf-F |
| Number Fins per inch: | 0.00 | | Mean Temperature Dif: | 1383 | F |
| Fin Height: | 0.000 | in | Gas HTC (hc): | 24.14 | B/h-sf-F |
| Fin Thickness: | 0.000 | in | Radiant HTC (hr): | 4.38 | B/h-sf-F |
| Fin Serrated Factor: | 0.000 | | Water HTC (hi): | 406.55 | B/h-sf-F |
| Fin ASME Material Group: | | | Convection Duty: | 29.614 | MMB/h |
| Water In From Section: | 3 | | Water Velocity: | 109.3 | ft/s |
| Water Out To Section: | 0 | | | | |

Evaporator Section 3, Group 1

| Evaporator Section 3, Group 1 | | | | | | |
|-------------------------------|--------|----|--------------------------|---------|----------|--|
| Tube Outside Diameter: | 2.000 | in | Tube Inside Diameter: | 1.706 | in | |
| Tube Min Wall Thickness: | 0.135 | in | Gas Inlet Temperature: | 1837 | F | |
| Tube Length: | 10.50 | ft | Gas Outlet Temperature: | 885 | F | |
| Finned Tube Length: | 10.50 | ft | Water Inlet Temperature: | 371 | F | |
| Tube ASME Material Group | : B | | Water Outlet Temperature | : 514 | F | |
| Number of Tubes Wide: | 13 | | Max Tube Temp (gas in): | 600 | F | |
| Number of Tubes Deep: | 60 | | Mean Wall Temperature: | 590 | F | |
| Fin Margin Temp Diff: | 0 | F | Max Fin Tip Temperature: | 600 | F | |
| Transverse Pitch: | 4.750 | in | Gas PD Surface Area: | 4288 | sft | |
| Longitudinal Pitch: | 4.000 | in | Gas Pressure Drop: | 3.722 | in H2O | |
| Tube Arrangement: | Inline | | Water Pressure Drop: | | | |
| Flow Direction: | | | Maximum Gas Velocity: | 110.2 | ft/s | |
| Number of Streams: | 0 | | Gas Specific Heat: | 0.310 | B/lb-F | |
| Outside Fouling Factor: | 0.0010 | | Overall HT Coef (U): | 18.82 | B/h-sf-F | |
| Inside Fouling Factor: | 0.0010 | | Mean Temperature Dif: | 749 | F | |
| Number Fins per inch: | 0.00 | | Gas HTC (hc): | 17.47 | B/h-sf-F | |
| Fin Height: | 0.000 | in | Radiant HTC (hn): | 2.57 | B/h-sf-F | |
| Fin Thickness: | 0.000 | in | Water HTC (hi): | 2000.00 | B/h-sf-F | |
| Fin Serrated Factor: | 0.000 | | Convection Duty: | 60.452 | MMB/h | |
| Fin ASME Material Group: | | | Maximum Heat Flux: | 29184 | Btu/sf | |
| Water In From Section: | 5 | | | | | |
| Water Out To Section: | 2 | | | | | |

Evaporator Section 4, Group 1

| Tube Outside Diameter: | 2.000 | in | Tube Inside Diameter: | 1.706 | in |
|--------------------------|--------|----|--------------------------|---------|----------|
| Tube Min Wall Thickness: | 0.135 | in | Gas Inlet Temperature: | 885 | F |
| Tube Length: | 10.50 | ft | Gas Outlet Temperature: | 764 | F |
| Finned Tube Length: | 9.55 | ft | Water Inlet Temperature: | 371 | F |
| Tube ASME Material Group | : В | | Water Outlet Temperature | : 514 | F |
| Number of Tubes Wide: | 12 | | Max Tube Temp (gas in): | 565 | F |
| Number of Tubes Deep: | 9 | | Mean Wall Temperature: | 560 | F |
| Fin Margin Temp Diff: | 0 | F | Max Fin Tip Temperature: | 633 | F |
| Transverse Pitch: | 4.750 | in | Gas PD Surface Area: | 1947 | sft |
| Longitudinal Pitch: | 4.000 | in | Gas Pressure Drop: | 1.271 | in H2O |
| Tube Arrangement: | Inline | | Water Pressure Drop: | 0.000 | psi |
| Flow Direction: | | | Maximum Gas Velocity: | | |
| Number of Streams: | 0 | | Gas Specific Heat: | 0.291 | B/lb-F |
| Outside Fouling Factor: | 0.0010 | | | | |
| Inside Fouling Factor: | 0.0010 | | - | | |
| Number Fins per inch: | 2.00 | | Gas HTC (hc): | | |
| Fin Height: | 0.500 | in | Radiant HTC (hn): | 0.93 | B/h-sf-F |
| Fin Thickness: | 0.105 | in | Water HTC (hi): | 2000.00 | B/h-sf-F |
| Fin Serrated Factor: | 0.000 | | Convection Duty: | 7.270 | MMB/h |
| Fin ASME Material Group: | | | Maximum Heat Flux: | 19128 | Btu/sf |
| Water In From Section: | | | | | |
| Water Out To Section: | 2 | | | | |

Economiser Section 5, Group 1

| LC | onomizee. | r secon | on o, Group r | | |
|--------------------------|-----------|---------|---------------------------|--------|----------|
| Tube Outside Diameter: | 1.500 | in | Tube Inside Diameter: | 1.173 | in |
| Tube Min Wall Thickness: | 0.150 | in | Gas Inlet Temperature: | 764 | F |
| Tube Length: | 11.00 | ft | Gas Outlet Temperature: | 318 | F |
| Tube ASME Material Group | : B | | Water Inlet Temperature: | 219 | F |
| Number of Tubes Wide: | 23 | | Water Outlet Temperature: | 371 | F |
| Number of Tubes Deep: | 14 | | Max Tube Temp (gas in): | 481 | F |
| Fin Marginal Temp Diff: | 0 | F | Mean Wall Temperature: | 469 | F |
| Transverse Pitch: | 3.500 | in | Max Fin Tip Temperature: | 620 | F |
| Longitudinal Pitch: | 4.500 | in | Min Tube Temperature: | 247 | F |
| Tube Arrangement: | Inline | | Min Fin Tip Temperature: | 282 | F |
| Flow Direction: | Counter | | Gas PD Surface Area: | 16294 | sft |
| Number of Streams: | 23 | | Gas Pressure Drop: | 2.089 | in H2O |
| Outside Fouling Factor: | 0.0010 | | Water Pressure Drop: | | |
| Inside Fouling Factor: | 0.0010 | | Maximum Gas Velocity: | 56.2 | ft/s |
| Number Fins per inch: | | | Gas Specific Heat: | 0.279 | B/lb-F |
| Fin Height: | 0.750 | in | Overall HT Coef (U): | 7.37 | B/h-sf-F |
| Fin Thickness: | 0.060 | in | Mean Temperature Dif: | 213 | F |
| Fin Serrated Factor: | | | | 12.20 | B/h-sf-F |
| Fin ASME Material Group: | В | | Radiant HTC (hr): | 0.41 | B/h-sf-F |
| Water In From Section: | 0 | | | | B/h-sf-F |
| Water Out To Section: | 3 | | Convection Duty: | 25.618 | MMB/h |
| | | | Water Velocity: | 4.8 | ft/s |
| | | | | | |

















